



## Investigation of sulfur poisoning of $CN_x$ oxygen reduction catalysts for PEM fuel cells

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### ARTICLE INFO

#### Article history:

Received 18 March 2011

Revised 23 August 2011

Accepted 22 September 2011

Available online 22 October 2011

#### Keywords:

$CN_x$

X-ray absorption spectroscopy

Oxygen reduction

Sulfur poisoning

Active site

### ABSTRACT

The role of the transition metal used during the growth of non-noble metal electrochemical oxygen reduction  $CN_x$  catalysts was investigated through sulfur treatment, a well-known poison for transition metal-based catalysts. The intent of sulfur poisoning was to show the existence of an electrocatalytic active site in  $CN_x$  that did not depend on iron. The sulfur treatment was shown to be effective on a platinum catalyst, as seen by the decreasing onset potential. The same treatment, however, not only showed no negative effect on the  $CN_x$  catalyst, but enhanced its performance, as seen by the increase in the onset potential. This suggests that, if there are iron-based active sites in these catalysts, they are either sulfur tolerant or they do not participate in the electrocatalytic oxygen reduction. The deposition of sulfur onto  $CN_x$  catalyst was verified by temperature-programmed oxidation and X-ray photoelectron spectroscopy. Iron K-edge X-ray absorption near edge structural analysis of the  $CN_x$  catalyst suggested that the iron phase, which was primarily composed of nanometer-sized metallic particles, was unchanged by sulfur poisoning, suggesting that the residual iron left in these materials is not catalytically accessible.

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### 1. Introduction

Fuel cells have the potential to radically alter the contemporary energy landscape, but many economic and technological challenges must first be overcome. Economically prohibitive loadings of platinum are used in the proton exchange membrane (PEM) fuel cell cathodes to overcome the slow kinetics of the oxygen reduction reaction (ORR).

Non-noble metal catalysts have been shown to have significant oxygen reduction activity and could potentially reduce or replace platinum in PEM fuel cells. Research on oxygen reduction reaction over non-noble metal electrocatalysts was inspired by naturally occurring organic macrocycles in hemoglobin where oxygen adsorption readily occurs at low temperatures. In hemoglobin, oxygen adsorbs onto an iron center (heme site) that is coordinated by four surrounding nitrogen functional groups at 37 °C [1]. It was discovered that heme-like molecules, such as iron phthalocyanines and macrocycles, were active for ORR in the fuel cell cathode, but quickly deactivated in acidic environments where the Fe– $N_x$  active sites are destroyed [2–5]. To improve the stability of these materials, pyrolysis, heat treatment in an inert atmosphere, above 600 °C was used to stabilize the organic macrocycles on a carbon support [3–15]. Although the pyrolysis step was found to completely destroy the coordinated metal active site, the catalyst materials

prepared through pyrolysis were found to be more active and stable than macrocycles, leading researchers to believe that a new active site had been formed during the heat treatment [16]. The structure of this new active site has not been definitively determined, although researchers have hypothesized a number of different sites ranging from metal atoms stabilized by nitrogen groups, to non-metallic sites grown catalytically by the presence of a metal during pyrolysis [3,12,14,17–19].

The high-temperature treatment used to stabilize non-noble metal catalyst materials facilitates the formation of all possible bonding configurations, thereby allowing many atomic arrangements any of which could be responsible for the ORR activity. It has been established that a carbon source, a transition metal, and a nitrogen source need to be present during pyrolysis to achieve high ORR activity [17,20–31], but the exact bonding configuration that facilitates high ORR activity is still debated.

We have previously shown that significant ORR activity can be achieved in a metal-free (<1 ppm Fe)  $CN_x$  catalyst, and in light of those findings, it was suggested that iron was not a part of the active site, but plays the role of a growth catalyst for carbon nanostructures [32,33]. Although the presence of multiple active sites, i.e., one with a metallic center and one without, cannot be ruled out, the activity observed over these materials being solely due to the presence of Fe centers in very low concentrations (100 ppm or less) is less likely. If this were the case, the intrinsic activity of these metal centers would be exceptionally high. In this paper, we adopt an exclusionary approach by attempting to

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deliberately poison the catalysts with sulfur to determine whether a transition metal is present in the active site for oxygen reduction in  $CN_x$  materials.  $CN_x$  catalysts prepared using a number of different transition metals during synthesis have been shown to have significant activity with the  $CN_x$  catalyst grown on Fe- or Co-containing media having the highest activity [19,34–38]. Sulfur is a well-known catalyst poison, which has been shown to deactivate iron-based catalysts for Fischer–Tropsch, water-gas shift, ammonia synthesis, ammonia decomposition, and iron carburization [39–42]. Binding reaction of  $H_2S$  with the ferric center of heme has also been reported [1,43]. Similarly, hydrogen sulfide treatment can be expected to have a similar poisoning effect on any iron-containing active sites present on non-noble metal ORR electrocatalysts. To the best of our knowledge, this is the first time there have been any reports on the sulfur poisoning attempts of  $CN_x$  oxygen reduction catalysts.

## 2. Experimental

### 2.1. Materials synthesis

The  $CN_x$  growth media was prepared by incipient wetness impregnation of 2wt% Fe onto a nanopowder magnesia support (Sigma–Aldrich) using an aqueous solution of iron (II) acetate (Sigma–Aldrich), followed by drying of the growth media overnight at 110 °C in air. Two grams of growth media was then weighed into a quartz calcination boat and placed inside of a quartz calcination tube in a high-temperature furnace. The calcination tube was purged with nitrogen at 150 mL/min for 30 min and then heated at 10 °C/min until 900 °C was reached. Upon reaching 900 °C, acetonitrile ( $CH_3CN$ , Fisher, Optima grade)-saturated nitrogen gas at 150 mL/min was streamed over the growth media for 2 h. After the 2 h of catalyst growth treatment, the system was cooled under nitrogen to room temperature. The resulting carbon nanostructures were washed in 1 M HCl at 60 °C to remove the magnesia support and any exposed iron, rinsed with excess deionized and distilled water with vacuum filtration, and dried in a convection oven at 110 °C. The resulting dry material is considered nitrogen-containing carbon ORR catalyst ( $CN_x$ ).

To study the effects of sulfur poisoning,  $CN_x$  was treated after catalyst growth in a variety of atmospheres. Between quartz wool plugs, 150 mg of  $CN_x$  was placed into a quartz reactor tube in a high-temperature furnace. The quartz tube was purged with nitrogen at 33 ml/min for 30 min and then heated at 10 °C/min until 350 °C was reached. At 350 °C, the catalyst was treated with 1050 ppm  $H_2S/N_2$  or 5.7%  $H_2/N_2$  at 33 ml/min for 2 h. At the end of 2 h of treatment, the system was cooled in nitrogen gas at 33 ml/min to room temperature. Control experiments were carried out over 20 wt.% Pt/Vulcan Carbon (BASF) that underwent the same treatment procedures.

### 2.2. Oxygen reduction activity testing

The ORR activity of catalysts was determined by electrochemical half-cell testing with a rotating disk electrode (RDE). Catalyst inks were prepared using a composition of 1:10:160 (by mass): catalyst: 5% Nafion in aliphatic alcohols: 100% ethanol. Inks were sonicated with low energy for 30 min. Three 5- $\mu$ L aliquots of catalyst ink were applied to a 0.1642  $cm^2$  glassy carbon disk, resulting in a catalyst loading of 426  $\mu$ g/ $cm^2$ . A model 636 RDE setup was connected to a Princeton Applied Research Bistat for the electrochemical testing. An Ag/AgCl (saturated KCl) reference electrode and a Pt wire counter electrode were used for the half-cell system. All reported potentials are referenced versus the normal hydrogen electrode (NHE). The half-cell electrolyte was 0.5 M  $H_2SO_4$ . It has

been reported that there is no significant difference in ORR testing of  $CN_x$  catalysts between  $H_2SO_4$  and  $HClO_4$  solutions [11,44]. It should be noted that although  $H_2SO_4$  is thought to poison platinum-based catalysts [45], since the electrochemical methods were identical for all Pt catalysts studied, the deactivation would be equivalent, making any activity differences attributable to the chemical treatments used.

ORR catalyst testing was performed using cyclic voltammetry (CV) on the glassy carbon disk. All CVs for  $CN_x$  were scanned from 1.2 V to 0.0 V to 1.2 V vs. NHE. The CVs for platinum were scanned from 1.2 V to 0.2 V to 1.2 V vs. NHE to prevent hydrogen evolution. To begin testing, the electrolyte was saturated with oxygen and disk CVs were run at 10 mV/s to remove any gaseous oxygen from the catalyst pores and fully wet the catalyst.

Prior to the collection of the background, the half-cell was purged with argon for 30 min to remove nearly all the dissolved oxygen. Disk CVs were run at a scan rate of 50 mV/s to eliminate impurities from the electrode surface. Immediately after the last scan, a disk CV was run at 10 mV/s while the assembly was rotating at 100 rpm to collect the background.

The electrolyte was, then, saturated with oxygen for 30 min to determine activity of the catalysts. Once again, disk CVs were run at a scan rate of 50 mV/s to eliminate impurities from the electrode surface. Immediately following the last scan, oxygen was bubbled through the electrolyte for 1–2 min to re-saturate the solution, following which a 1000 rpm oxygen-saturated electrolyte disk CV at 10 mV/s was performed. Additional CVs were run at 100 rpm and 0 rpm in oxygen-saturated electrolyte using a scan rate of at 10 mV/s.

To ensure that any possible contamination from Pt counter electrode did not affect the measurements taken in RDE apparatus, control experiments were performed where ORR activity of  $CN_x$  catalysts were measured in a RDE apparatus using a graphite counter electrode. The activity results did not show any change in activity, which could be ascribed to Pt contamination.

### 2.3. X-ray photoelectron spectroscopy

X-ray photoelectron spectroscopy (XPS) was used to examine the binding energies and environments of oxygen, nitrogen, carbon, and sulfur, when applicable, in the  $CN_x$  catalysts. A Kratos Ultra Axis Spectrometer with a monochromated aluminum anode source was used to collect a survey spectrum, O 1s, N 1s, C 1s, and S 2p regions for each  $CN_x$  catalyst sample. Analysis of the collected data was done on XPSPeak 4.1<sup>®</sup> using Shirley background for baseline correction and a combination of Lorentzian–Gaussian peaks for curve fitting. For quantitative comparison of the surface composition  $CN_x$  catalysts that underwent different treatments, the atomic sensitivity factors were used to correct the XPS peak areas for the relative sensitivity of the XPS instrument toward each species.

### 2.4. Temperature-programmed oxidation

Temperature-programmed oxidation (TPO) experiments were carried out using a mass spectrometer with gas chromatography interface (Thermo-Finnigan, Trace DSQ GC/MS, 2-1050 atomic mass units (amu)) to monitor the oxidation temperature and composition of the  $CN_x$  catalysts. For each run, 10 mg of  $CN_x$  catalyst was loaded into a quartz reactor tube with a quartz frit bed and was placed into a high-temperature, resistively-heated furnace (Carbolite, MTF 10/15/130), from which the exit stream was fed to the mass spectrometer. The temperature was ramped at 10 °C/min to 900 °C, while flowing 30 ml/min of 5%  $O_2$ /helium. Mass signal traces ( $m/z$ ) from 12 to 80 amu were monitored during the experiment.

## 2.5. X-ray absorption spectroscopy

The X-ray absorption fine-structure spectroscopy (XAFS) measurements were taken on the bending magnet beam line of the Dow-Northwestern-Dupont Collaborative Access Team (DND-CAT, Sector 5) at the Advanced Photon Source, Argonne National Laboratory. EXAFS for the iron carbide sample used for comparison was collected at The Materials Research Collaborative Access Team (MRCAT, Sector 10) of the Advanced Photon Source, Argonne National Laboratory. Measurements were taken in the transmission mode with ionization chambers optimized for maximum current with linear response.

Standard procedures were used to extract the XAFS data from the absorption spectra using WINXAS97 software [46]. Samples were ground and cast into self-supporting pellets. The XAFS data were collected at room temperature in air.

## 2.6. Transmission electron microscopy

An FEI Tecnai F20 XT Transmission Electron Microscope (TEM) operated at 200 kV was used to locate the iron phase within the  $CN_x$  catalyst. The material was prepared for imaging by sonicating a suspension of catalyst in ethanol, which was then deposited on a lacey formvar-carbon supported on a 200 mesh copper TEM grid.

## 3. Results and discussion

### 3.1. Effect of $H_2S$ on oxygen reduction activity

A hydrogen sulfide treatment was used to poison any iron-containing active sites present on  $CN_x$  catalysts. Pt/VC was also used for comparison. In previous reports, in the literature, it was shown that activity of Fe-containing  $CN_x$  materials was correlated with micropore volume (<2 nm), leading to the hypothesis that the ORR active site(s) was housed within Fe-/N-/C-type centers located in the micropores [47]. To effectively poison the proposed microporous Fe/N/C active site, the sulfur poison will need physical access to the sites while being chemically active. Oxygen has a collision diameter ( $\sigma_{O_2}$ ) of 3.467 Å, while hydrogen sulfide has a collision diameter ( $\sigma_{H_2S}$ ) of 3.623 Å [48]. This would suggest that hydrogen sulfide would have nearly the same micropore access as oxygen in  $CN_x$  catalyst. Furthermore, hydrogen sulfide is known to readily bind to the oxygen adsorption iron site in heme at 37 °C [1], and to poison Fe-based water gas shift catalysts in 300–450 °C range [42], so the  $H_2S$  treatment at 350 °C used in this study should be sufficient to bind and/or activate  $H_2S$  on the Fe-/N-/C-type active sites.

Oxygen reduction activity testing was carried out by cyclic voltammetry in a rotating disk electrode setup placed in an acidic solution to mimic the cathode environment in a direct methanol or hydrogen fuel cell. To isolate the heat treatment and reduction effects of  $H_2S$  poisoning, control experiments were carried out where separate samples of both  $CN_x$  and 20 wt.% Pt supported on Vulcan carbon were also heat-treated under the same conditions in a 5.7%  $H_2/N_2$  atmosphere. Fig. 1 shows a comparison of the oxygen reduction activity of an untreated Pt/Vulcan carbon with the same catalyst that underwent different treatments, i.e.,  $H_2$  or  $H_2S$ , prior to the testing of the activities. The decrease in activity shown for the platinum catalyst verifies that the  $H_2S$  treatment has a detrimental effect on the ORR activity under the treatment conditions used in this study. The decrease in activity can be observed in the lower onset potential (i.e., higher over potential) compared with the untreated platinum catalyst, Fig. 1 (inset). This observation is not surprising since sulfur has been previously reported to poison platinum ORR catalysts [41,49]. The hydrogen treatment is seen to increase the onset potential over the Pt/VC

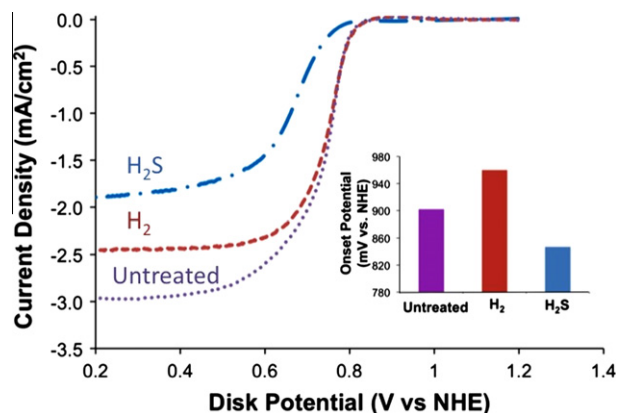


Fig. 1. Effect of  $H_2S$  treatment on the oxygen reduction activity of Pt/Vulcan carbon catalysts. Effect of  $H_2$  treatment is also included as a control experiment. Inset: comparison of onset potential.

catalyst. This observation is consistent with the expectation that reduced platinum sites would be more active for ORR. This control experiment with  $H_2$  also showed that any decrease in activity cannot be attributed to a heating effect. The differences in the limiting current could be due to the chemical treatment, affecting the coarseness or porosity of electrodes [50].

The experiments carried out with Pt catalysts were important in showing that the  $H_2S$  treatment was sufficient to impart a measurable poisoning effect, and thus validating the use of a similar procedure for  $CN_x$  catalysts.

Fig. 2 shows similar linear polarization curves for the untreated  $CN_x$  and catalysts that were treated under different atmospheres, i.e.,  $H_2$  or  $H_2S$ , prior to activity testing. The inset shows a comparison of the onset potentials. The sulfur poisoning treatment was found not to decrease the activity of  $CN_x$  oxygen reduction catalyst. On the contrary,  $CN_x$  ORR current density and onset potential were found to improve with  $H_2S$  treatment (Fig. 2). The greater current density suggests that electrode porosity or surface coarseness may have been altered by the  $H_2S$  treatment, allowing for increased mass transfer during oxygen reduction; however, the improved onset potential (i.e., lower over potential) demonstrates improved intrinsic activity. The  $H_2$  treatment in the control experiment also led to a higher onset potential, but the improvement was much more pronounced with  $H_2S$  treatment. This suggests that a secondary heat treatment in a reducing atmosphere can increase the activity of  $CN_x$ . The fact that there was no loss of activity

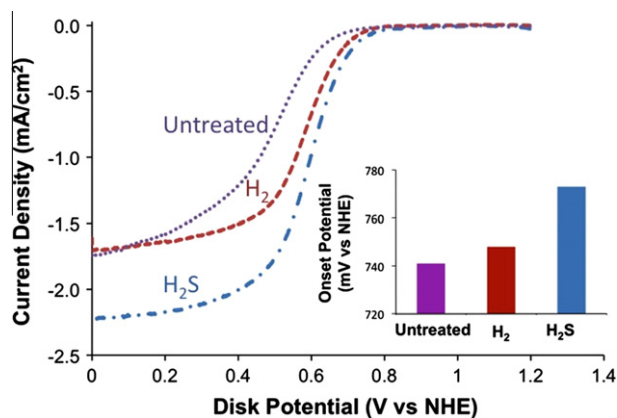


Fig. 2. Effect of  $H_2S$  treatment on the oxygen reduction activity of  $CN_x$  catalysts. Effect of  $H_2$  treatment is also included as a control experiment. Inset: comparison of onset potential.

following a treatment in  $\text{H}_2\text{S}$  is significant in showing that, if an iron-containing active site is present, either it is sulfur tolerant or does not participate in the electrocatalytic oxygen reduction. This result is not surprising considering it has already been shown that sulfur compounds introduced during pyrolysis could enhance  $\text{CN}_x$  catalyst growth, while the oxygen reduction activity remained largely unchanged [51]. Although it is not clear why an enhancement in  $\text{CN}_x$  ORR activity was observed with  $\text{H}_2\text{S}$  treatment, Chung et al. reported a similar activity increase on a non-precious metal catalyst synthesized by pyrolyzing cyanamide and iron sulfate [52]. If N-sites incorporated into the carbon nanostructure have ORR activity, it is conceivable that other heteroatoms such as sulfur can fulfill a similar role. The incorporation of heteroatoms such as phosphorus and sulfur into graphite has been demonstrated both experimentally and theoretically [53,54], and results suggesting ORR activity of other heteroatom-containing carbon structures have been reported [51,55–57]. The electronic structure calculations reported earlier [53] suggest an increased curvature in the graphite plane, due to heteroatom substitution. If the sulfur incorporation took place in the basal plane, one would expect such a “corrugation,” leading to a more defect-prone structure. It is also conceivable that the heteroatom substitution takes place at the edge sites, e.g., sulfur-occupying sites analogous to pyridinic nitrogen. At this point, it is not clear whether sulfur is replacing edge nitrogen or incorporating additional heteroatoms, and hence, changing the electron donor characteristics of graphite.

### 3.2. X-ray photoelectron spectroscopy

$\text{CN}_x$  catalysts that underwent heat treatment under different atmospheres were further characterized with XPS and temperature-programmed oxidation experiments to investigate the effect of such treatments on the surface and bulk properties of these catalysts and to determine the extent and location of sulfur incorporation to the carbon phase of the  $\text{CN}_x$  catalysts. The sulfur poisoning of the iron phase in  $\text{CN}_x$  catalyst was further studied by X-ray absorption spectroscopy.

Iron and magnesium were not detectable in the survey scans of any of the  $\text{CN}_x$  catalysts studied. This finding is consistent with our previous reports [58] and suggests that the acid washing step for  $\text{CN}_x$  fabrication removed most of the surface iron and magnesia. The XPS analysis of  $\text{CN}_x$  catalysts found similar nitrogen species surface compositions, regardless of the treatment (Fig. 3). Fig. 4 shows a comparison of the X-ray photoelectron spectra in the S 2p region for an  $\text{H}_2\text{S}$ -treated and an untreated  $\text{CN}_x$  catalyst. Although the intensity in this region is low due to the low intrinsic atomic sensitivity of the instrument for sulfur, photoelectron peaks arising from the presence of sulfur species can be seen in the S 2p envelope for the  $\text{H}_2\text{S}$ -treated catalyst. Deconvolution for providing insights to the nature and relative surface concentration of sulfur species was difficult due to weakly resolved envelope. However, it is possible to discern three different photoelectron peaks located at 161 eV, 165 eV, and 169 eV, which can be associated with sulfur species in sulfide ( $\text{S}^{2-}$ ), sulfite ( $\text{SO}_3^{2-}$ ), sulfate ( $\text{SO}_4^{2-}$ ) environments, respectively [59]. It should be noted that the splitting between  $2p_{3/2}$  and  $2p_{1/2}$  was not observed for the S 2p envelope due to small spin orbit splitting for sulfur (1.18 eV). Formation of sulfite and sulfate species can be associated with interaction of adsorbed sulfur with oxygen from ambient air during sample transfer, although an interaction between the sulfur- and the oxygen-containing functional groups present on the  $\text{CN}_x$  catalysts, leading to formation of sulfite species cannot be ruled out.

The elemental surface compositions of the  $\text{CN}_x$  samples determined from the quantitative analysis of XPS data are presented in Table 1. The results showed a redistribution of the elemental

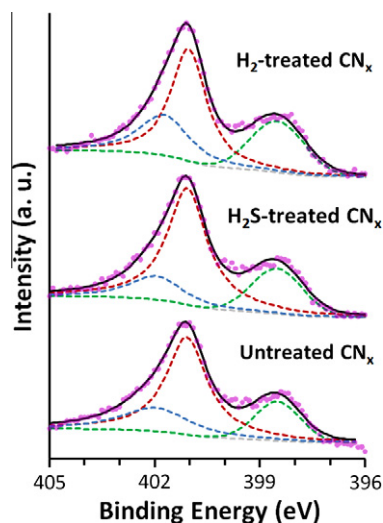


Fig. 3. X-ray photoelectron spectra in the N 1s region for untreated and heat-treated  $\text{CN}_x$  catalysts under different atmospheres.

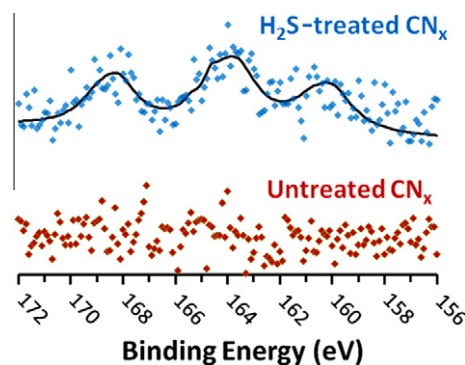


Fig. 4. X-ray photoelectron spectra of the S 2p region for untreated and  $\text{H}_2\text{S}$ -treated  $\text{CN}_x$  catalysts under different atmospheres.

surface concentration with  $\text{H}_2\text{S}$  treatment. The relative amount of surface oxygen was less for  $\text{CN}_x$  catalysts exposed to a reducing treatment. The reducing atmosphere used in  $\text{H}_2$  and  $\text{H}_2\text{S}$  treatments can account for this change. The relative amounts of different N species were also seen to change in favor of pyridinic nitrogen. However, small amount of sulfur was also detected on the surface of  $\text{H}_2\text{S}$ -treated sample. There have been previous reports suggesting that changes in the oxygen [60] and nitrogen [24,61] surface species can affect ORR electrocatalytic activity. It is difficult to discern which of these changes, if any, have contributed to the improved performance. It is possible that there may be multiple factors contributing to the change in activity, such as increase in relative surface concentrations of edge nitrogen sites as well as incorporation of sulfur atoms in the graphite matrix. Especially, the latter would be expected to change the electron donor characteristics of carbon. It should also be noted that the change in the performance of  $\text{CN}_x$  catalysts does not only manifest itself through the improved onset potential, but also through the increased limiting current. The latter can be attributed to changes in the textural properties, hence mass transfer characteristics, of the catalyst. It is possible that the  $\text{H}_2\text{S}$  treatment could lead to defects in the graphite structure due to the larger size disparity between the carbon and the sulfur. It is also conceivable that  $\text{H}_2\text{S}$  could lead to increased pore volumes that would enhance the mass transfer characteristics [62,63].

**Table 1**  
Compositional analysis of CN<sub>x</sub> catalysts from X-ray photoelectron spectroscopy.

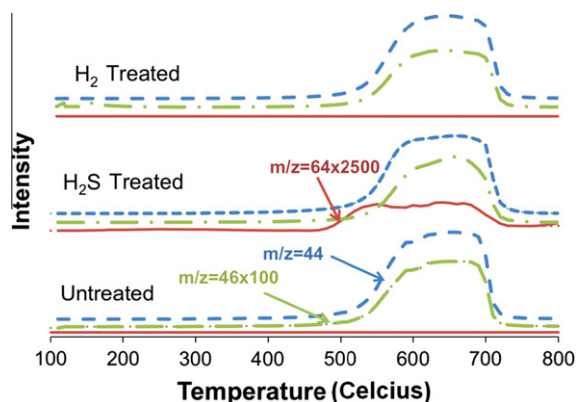
	O 1s (%)	N 1s (%)		C 1s (%)		S 2p (%)
	532.9 eV	398.8 eV	401.2 eV	402.0 eV	200.1 eV	163.5 eV
Untreated	3.8	1.4	4.5	1.7	88.6	0.0
H <sub>2</sub> S treated	2.4	1.7	3.5	0.9	91.3	0.2
H <sub>2</sub> treated	2.7	1.8	3.8	1.9	89.8	0.0

### 3.3. Temperature-programmed oxidation

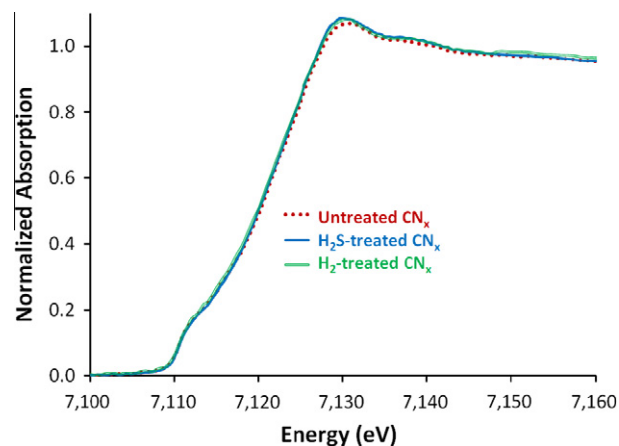
Temperature-programmed oxidation experiments were carried out over the untreated CN<sub>x</sub> catalyst as well as catalysts that were heat-treated under different atmospheres (Fig. 5). Regardless of the pretreatment conditions, the CO<sub>2</sub> ( $m/z=44$ ) and NO<sub>2</sub> ( $m/z=46$ ) traces closely followed each other and broad evolution bands for these species, which are associated with the decomposition of the CN<sub>x</sub> structure, were observed in 510–720 °C region. Over the H<sub>2</sub>S-treated catalyst, evolution of SO<sub>2</sub> ( $m/z=64$ ) that is concomitant to CO<sub>2</sub> and NO<sub>2</sub> was observed. This indicates that sulfur species that were retained on the surface after the H<sub>2</sub>S pretreatment were strongly bonded to the surface rather than being physically adsorbed.

### 3.4. X-ray absorption spectroscopy

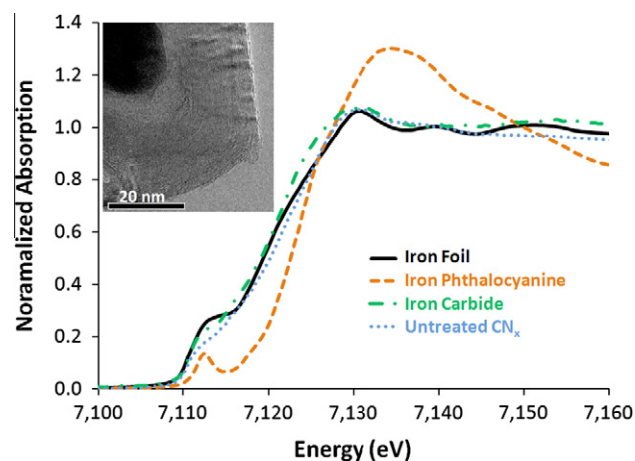
Since a transition metal improves the pyrolytic formation of the non-noble metal active site, it is difficult to ascertain the role of iron in ORR activity. X-ray absorption spectroscopy was used to probe the local bonding environment of the iron in CN<sub>x</sub> oxygen reduction catalysts. The XANES spectra for all CN<sub>x</sub> catalysts, Fig. 6, were nearly identical regardless of the post-synthesis treatment conditions, indicating that the local Fe structure is unchanged by H<sub>2</sub>S treatment. All CN<sub>x</sub> XANES spectra appeared to strongly resemble iron in the metallic or carbide phase, Fig. 7. None of the CN<sub>x</sub> samples studied resembled the iron phthalocyanine standard, which is similar to the nitrogen-bonded transition metal active site proposed by some researchers [19,64,65]. TEM of CN<sub>x</sub> catalysts revealed iron entirely encased within several carbon sheets, Fig. 7, inset. Since the iron phase is isolated from the chemical treatments by layers of carbon, it is not surprising that the Fourier transform obtained at the Fe K-edge and  $k^2$ -weighted EXAFS displayed a nearly identical local bonding environment for untreated and H<sub>2</sub>S-treated CN<sub>x</sub>, Fig. 8. The iron contained within CN<sub>x</sub> has a small metallic phase and an iron phase bonded to a lighter element (nitrogen, oxygen, and/or carbon). It can be seen that



**Fig. 5.** Evolution of CO<sub>2</sub> ( $m/z=44$  amu), NO<sub>2</sub> ( $m/z=46$  amu), and SO<sub>2</sub> ( $m/z=64$  amu) as a function of temperature during temperature-programmed oxidation of untreated, H<sub>2</sub>S-, N<sub>2</sub>-, and H<sub>2</sub>-treated CN<sub>x</sub>.



**Fig. 6.** XANES Fe K-edge spectra for untreated, H<sub>2</sub>S-, and H<sub>2</sub>-treated CN<sub>x</sub>.



**Fig. 7.** XANES Fe K-edge spectra for iron foil, iron phthalocyanine, iron carbide and untreated CN<sub>x</sub>.

untreated CN<sub>x</sub> Fe-Fe bond length is less than that of bulk iron, Fig. 9. This is likely due iron particles being much smaller in CN<sub>x</sub> catalyst than of a bulk iron foil. The iron-iron bonding shoulder at  $\sim 1.5$  Å in CN<sub>x</sub> catalyst coincides with Fe-N bond distance in iron phthalocyanine, but also aligns with the Fe-C bond distance in iron carbide. Due to the similar scattering spectra of 2p elements, it cannot be determined whether the CN<sub>x</sub> peak at  $\sim 1.5$  Å is due to an iron nitrogen, carbon, or oxygen bond. The EXAFS for iron carbide displayed the same peak structure and locations as the CN<sub>x</sub> catalysts studied. This is in agreement with an investigation into the CN<sub>x</sub> iron phase through Mössbauer spectroscopy, which revealed iron to consist of a metallic phase (a paramagnetic  $\gamma$ -Fe phase, which would be unstable in air) and a cementite phase (Fe<sub>3</sub>C), which is likely to be formed during the carbon fiber growth [58]. Working iron catalysts are often a complex mixture of iron

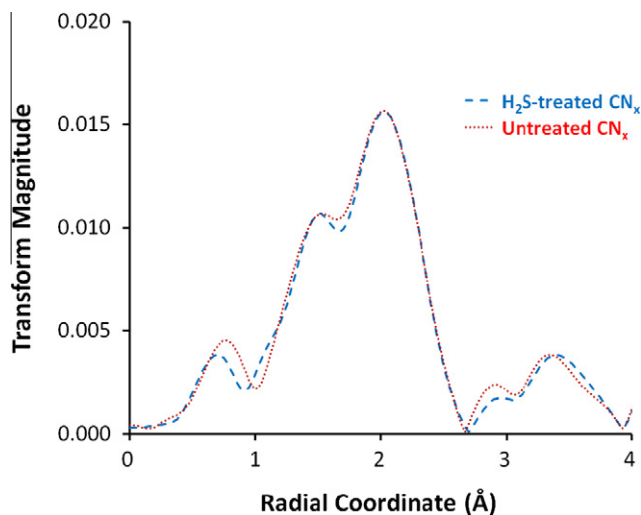


Fig. 8. EXAFS Fe K-edge spectra for H<sub>2</sub>S-treated and untreated CN<sub>x</sub>.

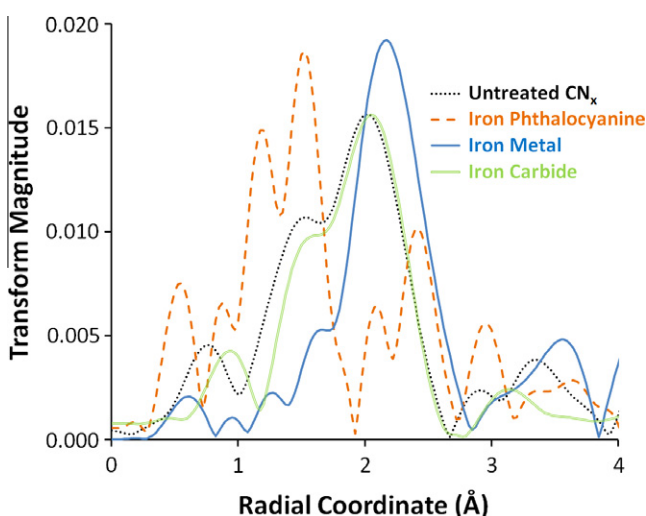


Fig. 9. EXAFS Fe K-edge spectra for untreated CN<sub>x</sub>, iron phthalocyanine, iron metal, and iron carbide.

carbide compounds, often containing a fraction of iron oxides [66]. An EXAFS theoretical structural model was prepared by Jacobs et al. using *ab initio* multiple scattering calculations of X-ray absorption fine structure for cementite (Fe<sub>3</sub>C), Hägg carbide (Fe<sub>5</sub>C<sub>2</sub>), ε-carbide (Fe<sub>3</sub>C), and η-carbide (Fe<sub>2</sub>C) to generate the Fourier transform magnitude versus bond distance for the iron K-edge in order to characterize the iron carbides present in Fischer–Tropsch synthesis catalysts [66]. CN<sub>x</sub> oxygen reduction electrocatalyst resembles a combination of the ε-carbide (Fe<sub>3</sub>C) and Hägg carbide (Fe<sub>5</sub>C<sub>2</sub>) when compared to the simulated carbide EXAFS spectra. Although CN<sub>x</sub> catalysts are grown in a reducing atmosphere, the presence of iron oxides cannot be ruled out.

#### 4. Conclusions

A sulfur poisoning treatment was performed on both platinum and CN<sub>x</sub> oxygen reduction catalysts to investigate the role of the transition metal in the CN<sub>x</sub> ORR active site. The intent of sulfur poisoning treatment was to effectively eliminate iron from the proposed electrocatalytic oxygen reduction active sites of CN<sub>x</sub>. The sulfur treatment was found to reduce ORR activity on the platinum

catalyst, which demonstrated the validity of the sulfur poisoning treatment. The H<sub>2</sub>S treatment was found to increase the activity on the CN<sub>x</sub> catalyst. The incorporation of sulfur into the CN<sub>x</sub> catalyst was verified by TPO and XPS spectra. The iron phase within the CN<sub>x</sub> catalysts was investigated with X-ray absorption and was found to be similar for the treatments studied, suggesting that iron was not catalytically accessible. XANES analysis of the CN<sub>x</sub> Fe K-edge showed the iron phase in CN<sub>x</sub> to be mostly metallic with possible contributions from a carbidic phase. No spectra resembled the iron macrocycle standard, which is similar to the hypothesized nitrogen-bonded transition metal ORR active site.

The source of the increase in ORR activity observed over the CN<sub>x</sub> catalyst following H<sub>2</sub>S treatment is not clear, but it may be due to multiple factors, including creation of new active sites associated with sulfur or creation of defects in the graphite matrix due to size disparity between carbon and sulfur. It is also likely that the H<sub>2</sub>S treatment may be changing the mass transfer characteristics of the catalyst by increasing porosity, and hence changing the limiting current.

#### Acknowledgments

The authors acknowledge the financial support for this work from US Department of Energy Basic Energy Sciences through the Grant DE-FG02-07ER15896. Portions of this work were performed at the DuPont–Northwestern–Dow Collaborative Access Team (DND-CAT) located at Sector 5 of the Advanced Photon Source (APS). DND-CAT is supported by E.I. DuPont de Nemours & Co., The Dow Chemical Company and the State of Illinois. Use of the APS was supported by the US Department of Energy, Office of Science, Office of Basic Energy Sciences, under Contract No. DE-AC02-06CH11357. The authors also acknowledge the NSF support for acquisition of the XPS system under NSF-DMR Grant #0114098.

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